

#### CO-FIRING & FUEL CHARACTERISATION The Reuse of Spent Mushroom Compost and Coal Tailings for Energy Recovery



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#### Overview

- Project aims and objectives
- Reusing wastes as a source of energy
- Typical emissions to the air
- Waste Incineration Directive
- Experimental results:
  - ~ material characterisation
  - ~ pelletisation
  - ~ fluidised-bed combustion of fuel pellets
- Discussion and conclusions



# **Project Aims and Objectives**

- To divert spent mushroom compost from landfill and aid the cleaning of land contaminated by coal tailings by generating a source of renewable, sustainable fuel
- To evaluate ways in which SMC and coal tailings can be utilised to produce energy
- To investigate and characterise the emissions produced from the thermal treatments of these wastes



# Wastes as a Source of Energy

- Reusing wastes for energy recovery can mitigate the impacts of unsustainable energy generation and waste management
- 1. Spent mushroom compost (SMC) an agricultural waste from mushroom farms





# Wastes as a Source of Energy

- Reusing wastes for energy recovery can mitigate the impacts of unsustainable energy generation and waste management
- 2. Coal tailings an industrial waste produced during coal cleaning processes





# **Typical Emissions to the Air**

- Solid-phase pollutants: ash
- Gas-phase pollutants include:
  - ~ CO and CO<sub>2</sub>
  - ~ acid gases NOx, SOx and HCI
  - ~ dioxins, furans, UHCs, VOCs and PAHs
- Problems: greenhouse gases, ozone depletion, acid rain, photochemical smog, carcinogenic/toxic
- Abatement and control to meet legislation



# **Waste Incineration Directive**

- Waste Incineration Directive WID
- Concerns the incineration of hazardous and non-hazardous waste
- Outlines limits for various pollutants:
  - ~ solid: flyash
  - ~ gaseous: NOx, SOx and HCI
- The combustion of SMC-coal tailing pellets must comply with this legislation



## **Material Characterisation**

ANALYSIS		COAL TAILINGS	SMC SUBSTRATE	SMC CASING
Moist	ure (%)	~ 40	65.70	68.56
Proximate Analysis (%)	Ash	41.25	26.89	28.87
	Volatile	20.51	61.80	60.18
	Fixed Carbon	38.24	11.31	10.95
Ultimate Analysis (%)	Carbon	47.87	35.13	35.72
	Hydrogen	2.90	3.59	3.01
	Nitrogen	1.01	2.85	1.11
	Chlorine	-	0.51	0.70
	Sulphur	1.38	2.95	2.16
CV (MJ/kg)	GCV, ar	11.91	4.94	4.33
	GCV, dry	19.85	14.11	12.37



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## **Pelletisation of Wastes**

PELLETISATION PARAMETER	OPTIMUM	
Moisture Content	10-11 %	
Minimum Pressure	2500 psi / 17 MPa	
Maximum Pressure	6000 psi / 41 MPa	
SMC:Coal tailing Ratio	50:50 wt%	
Binder	Starch	
Amount of Binder	1 wt%	
Temperature	45-75 °C	
Length of Steam Conditioning	5 mins	



#### **Thermal Treatments EXPERIMENTS**

- Combustion tests in a laboratory-scale fluidised-bed and a packed-bed:
  - ~ combustion of SMCcoal tailing pellets
  - ~ combustion of raw, dried SMC
- Gasification and pyrolysis of SMC

#### RESULTS

- Pellet combustion performed better
- Fluidised-bed combustion was more efficient than in both cases
- Fluidised-beds are better suited for high ash-content fuels



#### **Fluidised-bed Combustor**







Air Ratio



# **Evaluation of Combustion**

- Small-scale nature of the reactor meant inherent inefficiencies
- Scale-up of the reactor
  - a deeper bed can be used whilst maintaining a bed-depth-to-diameter ratio of 1
  - ~ increase efficiency
- Secondary air jets
  - high-speed, turbulent secondary air to optimise fuel-oxidiser mixing to complete burnout of fuel and residual gases
  - ~ lower CO, prompt NOx and combustible material



## **Gaseous Emissions**

	NOx	SOx	HCI
Range	2.1 - 58.4 ppm	2.35 - 41.69 ppm	0.88 - 16.88 ppm
Average	10-20 ppm	12 ppm	5.3 ppm
Maximum	91 mg/m <sup>3</sup>	123 mg/m <sup>3</sup>	25 mg/m <sup>3</sup>
WID Limits	200-400 mg/m <sup>3</sup> (~257 ppm)	50 mg/m <sup>3</sup> (~19 ppm)	10 mg/m <sup>3</sup> (~6.7 ppm)
Ash	N not abundant in the $ash - N_2O?$	S concentrated in ash – 15,000 mg/kg	CI concentrated in ash – 535 mg/kg



#### **Particulate Pollutants**

COMPONENT (mg/kg)	FUEL PELLETS	FLYASH
Flyash as % of Ash in Pellets	-	78.95
Alkali Index (kg-alkali/GJ)	-	0.235
AI	2500	45000
Fe	5604	37250
K	8364	20625
Na	1123	3750
Р	3121	5237.5
S	11702	15300
Si	1487	3137.5
Ash Fusion Temperatures (°C)	-	1272



# **Discussion and Conclusions (1)**

- Fluidised-bed combustion is the best way to recovery energy from these wastes, after drying and pelletisation
- Combustion efficiency could be high (up to 98 %) using appropriate conditions
- Efficiency could be further improved by:
  - ~ using turbulent secondary air to aid mixing
  - ~ an industrial-scale reactor with a deeper bed
  - ~ reduce CO, prompt NOx and unburned material



# **Discussion and Conclusions (2)**

- Characterisation identified potential pollutants
- NOx, SOx and HCI were minimal compared to the initial concentrations of N, S and CI
  - ~ NOx emissions were below regularity limits
  - ~ SOx and HCI did **not** conform to WID
- Flyash removal needed to comply with WID
  - ~ alkali metal oxides = slagging and fouling
  - ~ AI, Fe, Si and CI = ash agglomeration
  - ~ temperatures lower than those of ash fusion



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