



The University of  
Nottingham



# The EPSRC OxyCAP Project



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# Summary

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- ❑ The Oxy-CAP UK Consortium
- ❑ Gaps in the Knowledge of Oxy-fuel Technology
- ❑ Project Objectives
- ❑ Project Activities - Examples
- ❑ Conclusions and What Next?

# The OxyCap Consortium

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## Oxyfuel Combustion - Academic Programme for the UK

(£1,789,493 from EPSRC-EON)

01/11/2009

- Project Partner:



**EPSRC**

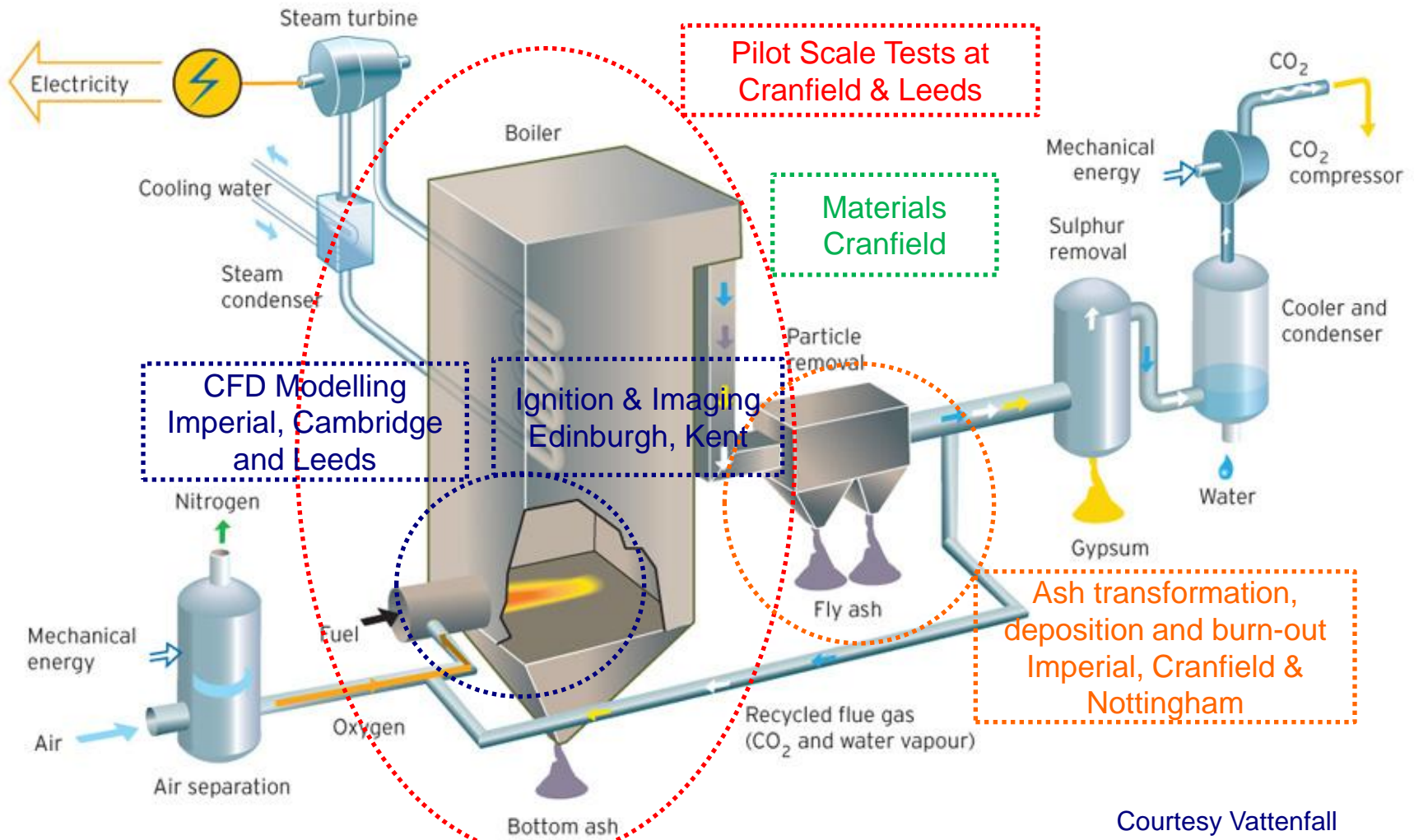
Engineering and Physical Sciences  
Research Council

# Some Knowledge Gaps in Oxycoal PF Combustion - 2009

- ❑ **Combustion behaviour**; impact of different coals on ignition behaviour, impact of varying recycle, modelling, monitoring, etc.
- ❑ **Optimum recycled flue gas (RFG) ratio**; to achieve similar combustion and heat transfer characteristics to an air fired operation.
- ❑ **Carbon burnout**; this data are only limited to a certain range of coal in the pilot scale studies.
- ❑ **Ash formation, slagging and fouling**; the effect of CO<sub>2</sub>-rich atmosphere on ash formation
- ❑ **Materials**; the impact of varying boiler and recycle environments on materials – water wall/superheater corrosion, acid dew-point corrosion
- ❑ **Fine particulates, SO<sub>3</sub>, NO<sub>x</sub>, trace metal emissions**; differences in conversion of fuel-S to SO<sub>2</sub>, SO<sub>3</sub> etc. and sulphur remaining in ash, levels of unburned carbon, condensates in recycle, etc.
- ❑ **Radiative Heat Flux measurements**; changes in heat flux with operating conditions
- ❑ **Etc.**

# Oxy-Cap Research Themes

## Oxyfuel ( $\text{O}_2/\text{CO}_2$ recycle) combustion capture



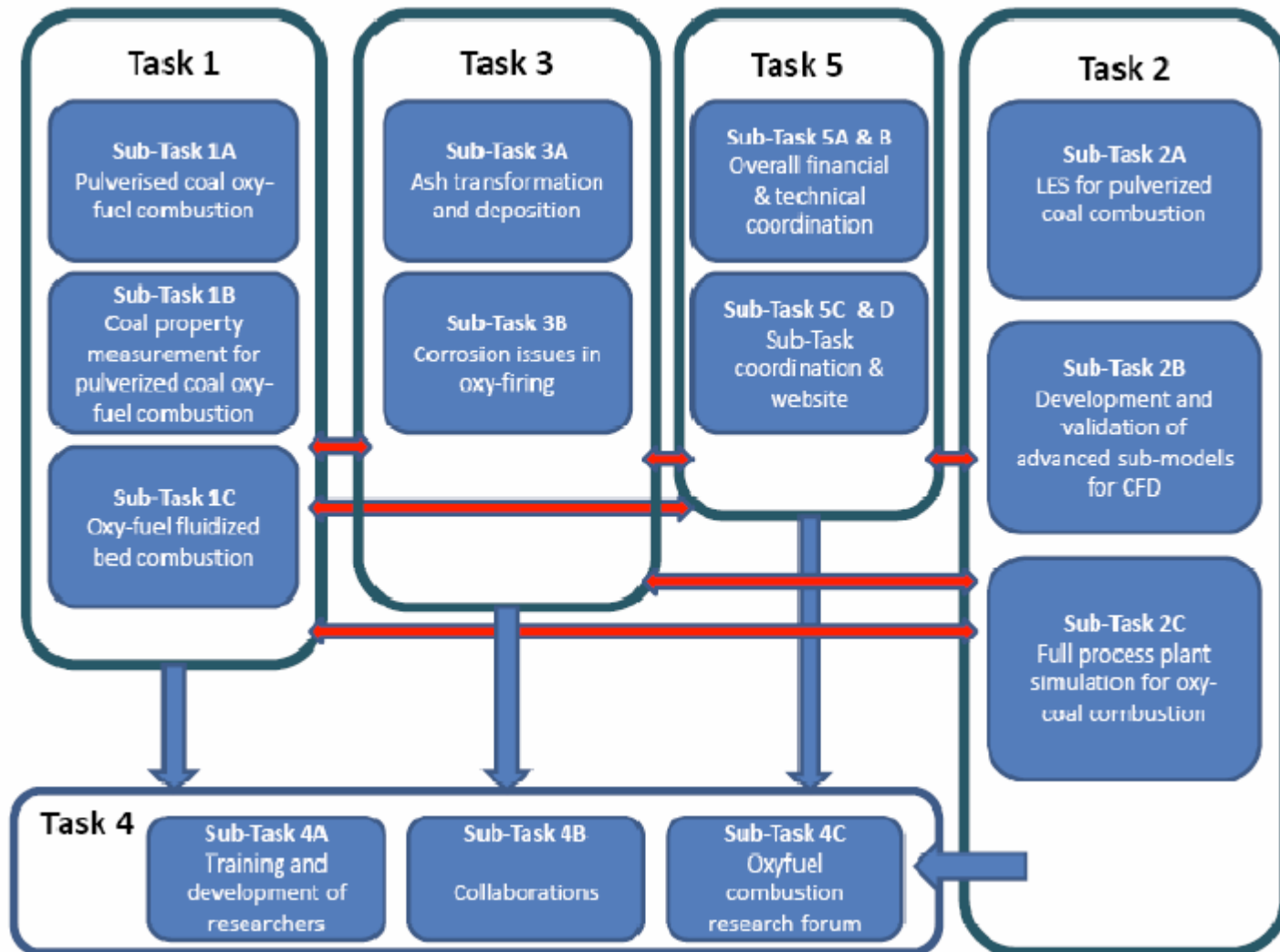
Courtesy Vattenfall

# OxyCap Objectives

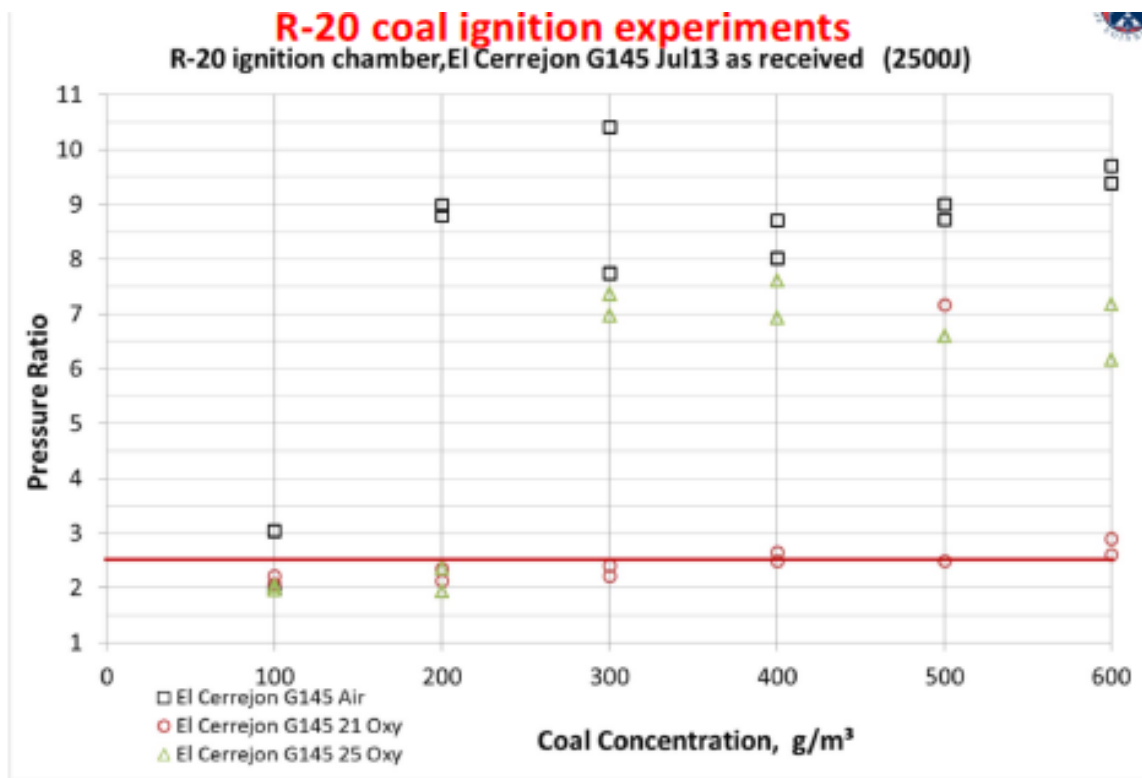
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- Develop a new generation of large-eddy simulation (LES) based, CFD models for coal combustion
- Develop a validation and verification environment that integrates experimental results
- Develop computational sub-models for key areas e.g. radiation, particle ignition, particle
- Measure the effect of the partial pressures of O<sub>2</sub> and CO<sub>2</sub> on oxy-coal combustion phenomena and establish novel experimental techniques for testing new coals and further sets of combustion conditions
- Analyse the interaction of oxy-combustion products with boiler materials, based on realistic flue gas environments and ash slagging behaviour under oxyfuel combustion conditions
- Increase UK advanced scientific capacity in this area

# Oxy-CAP UK Tasks Distribution



Coal/biomass dust ignition tests in oxyfuel atmospheres carried out at the University of Edinburgh.

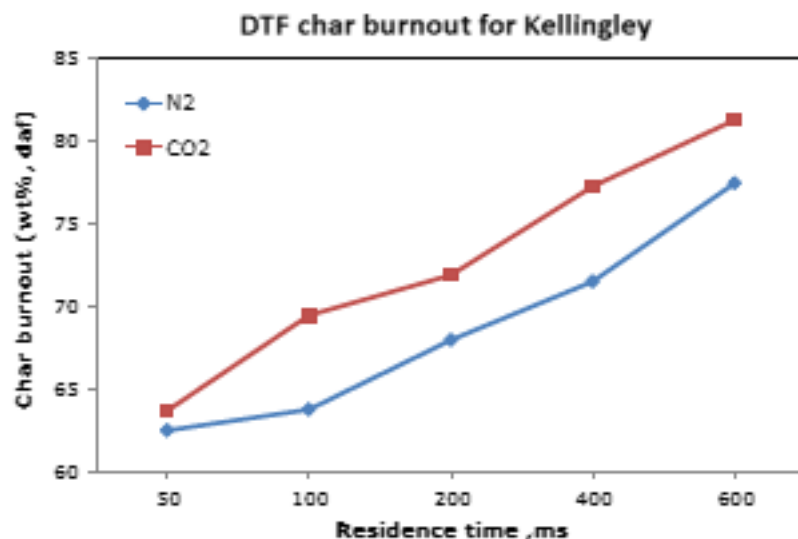
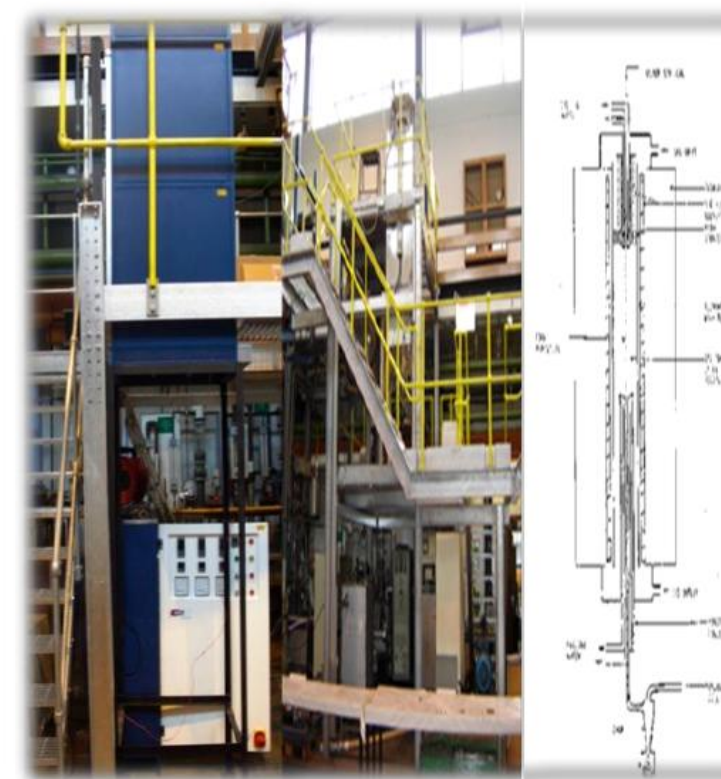


Ignition negative for all concentrations at 21 Oxy. Negatives for 25 Oxy 100-200 g/m³

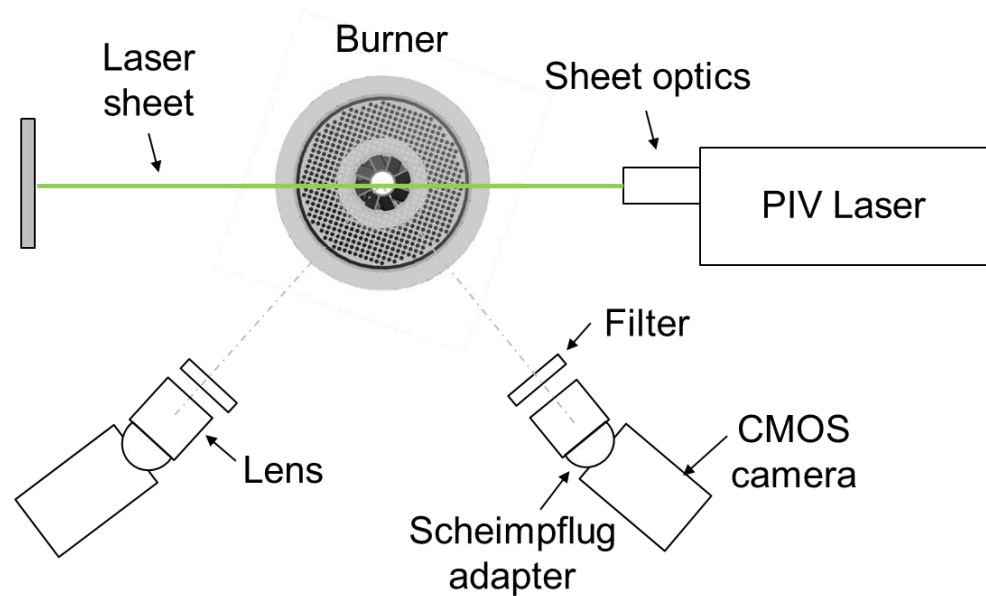
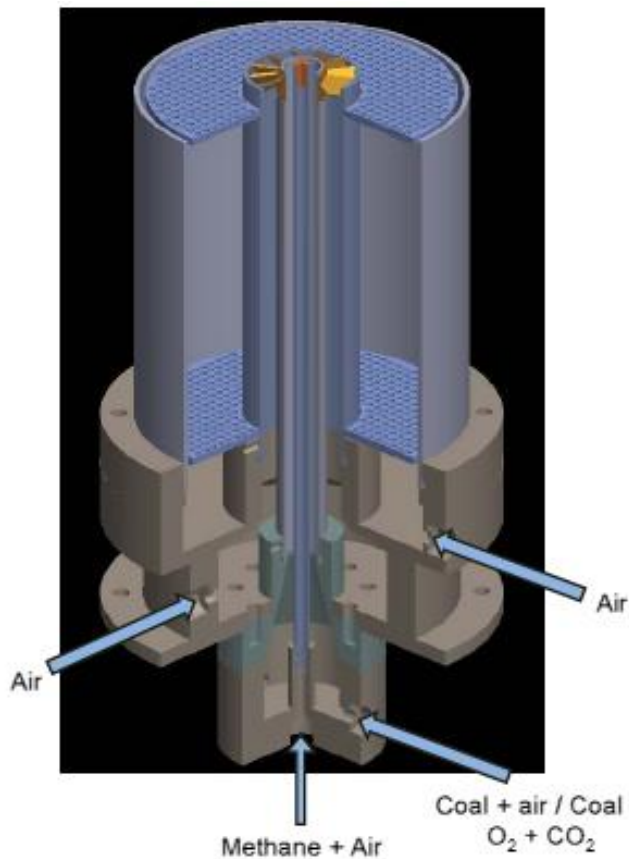


Ignition Test Chamber

- ❑ The impact of  $\text{CO}_2$  and steam on devolatilisation and char burn-out in relation to normal air firing is being assessed by a comprehensive drop tube furnace (DTF) programme at the University of Nottingham.
- ❑ The DTF operates up to  $1450^\circ\text{C}$  which is high enough to achieve the maximum volatile matter yields for coals with relatively short residence times.
- ❑ The results have indicated the enhanced volatile matter yields and char burn-out rates that can be achieved in  $\text{CO}_2$ .



## Oxy-Coal combustion in a $\text{CH}_4/\text{O}_2/\text{CO}_2$ burner (Experimental work and providing data for LES modelling)



LDV	PIV
System: Dantec Dynamics	System: LaVision
Probe volume: 0.91 X 0.14 X 0.14 mm <sup>3</sup>	Imaging area: 60.5 X 52.4 mm <sup>2</sup>
Data rate: ~10,000 Hz	Data rate: 3,000 Hz
Samples: 10,000	Samples: 4,096

High-speed stereo particle image velocimetry

# Coal Flame and OH\*/CH\* Images



UNIVERSITY OF  
CAMBRIDGE



Pilot  
flame



Plain  
Air



21% O<sub>2</sub>  
79% CO<sub>2</sub>



25% O<sub>2</sub>  
75% CO<sub>2</sub>



30% O<sub>2</sub>  
70% CO<sub>2</sub>



Plain  
Air

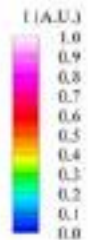
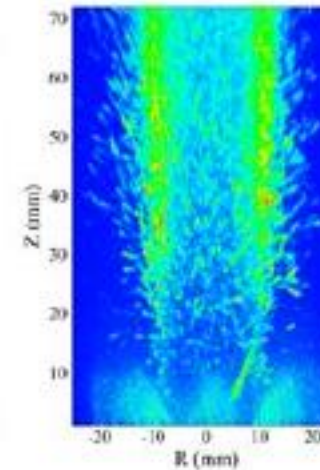
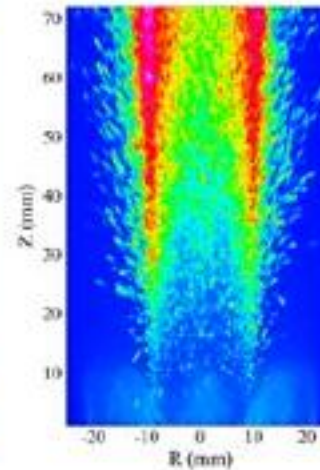
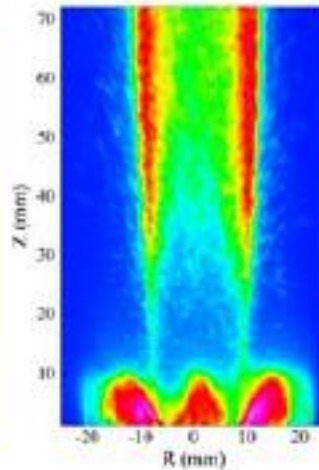
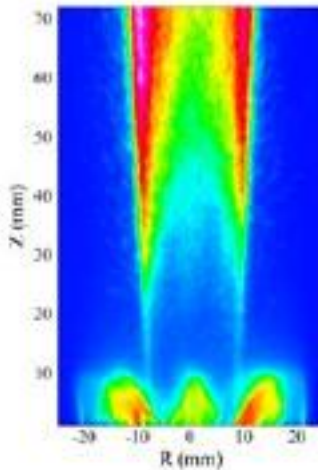
OH\* Mean

CH\* Mean

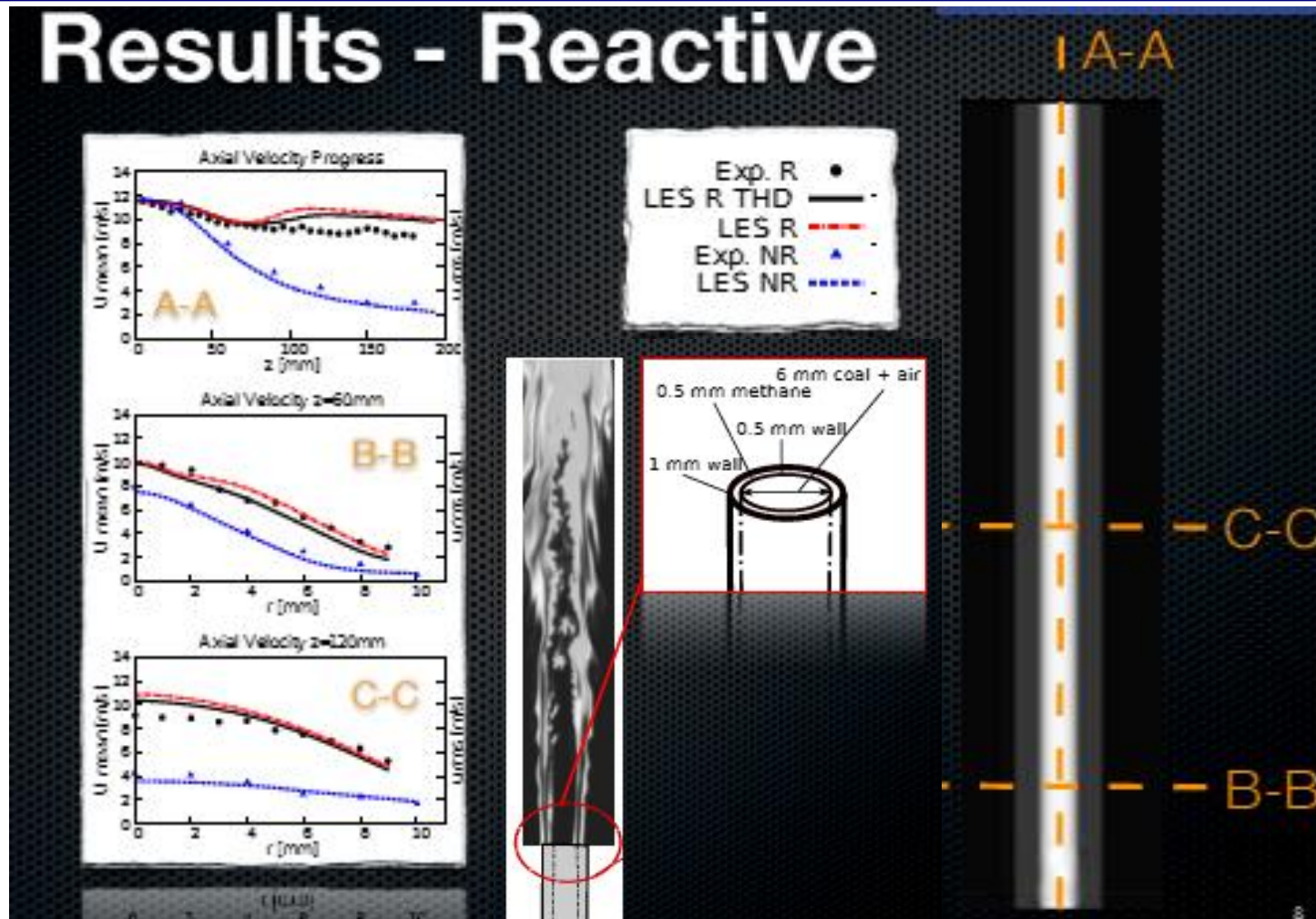
OH\* RMS

CH\* RMS

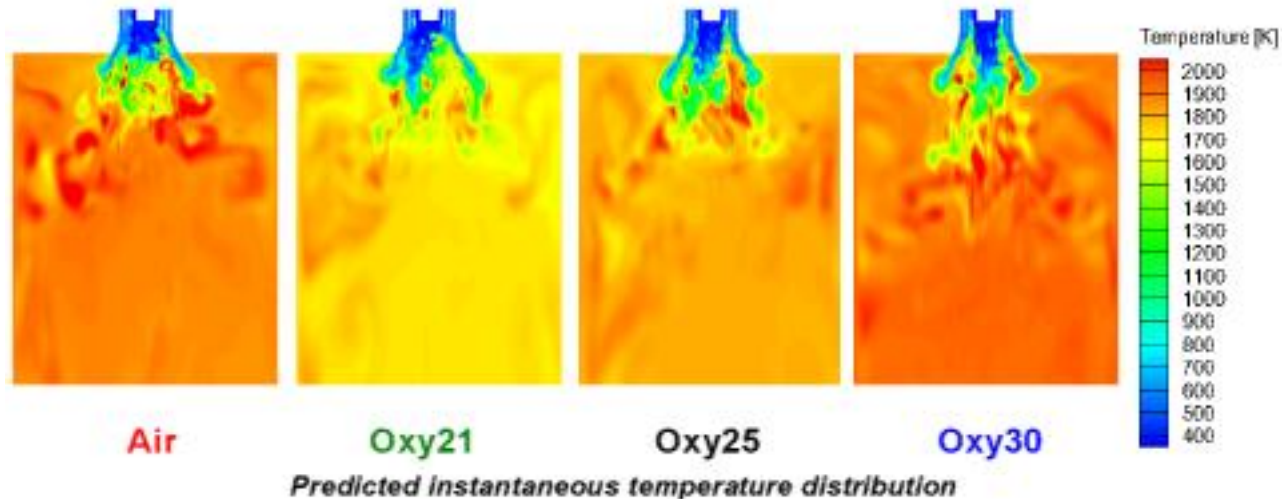
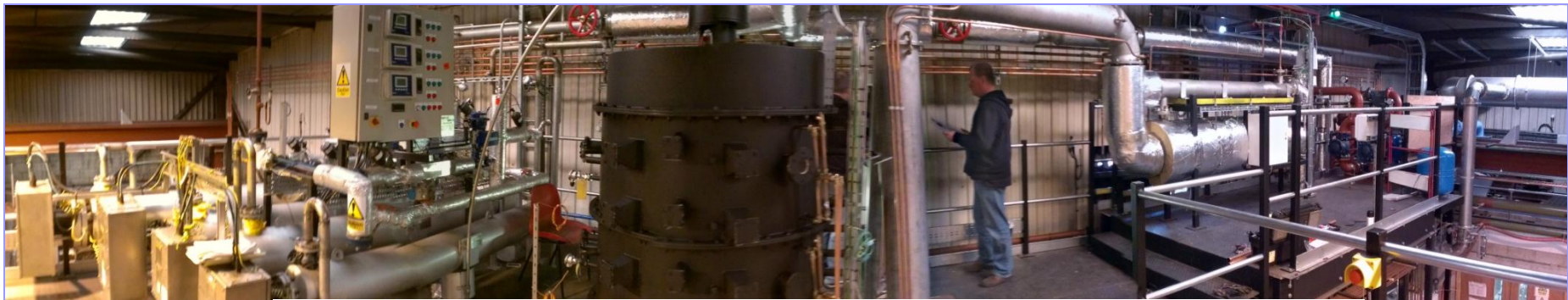
21% O<sub>2</sub> / 79% CO<sub>2</sub>



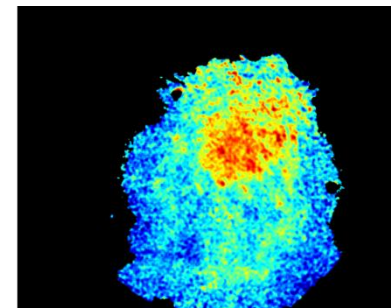
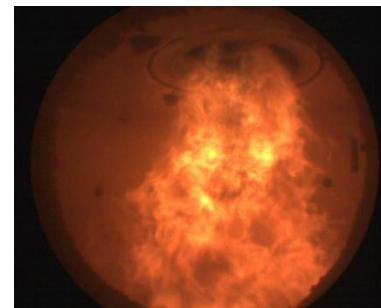
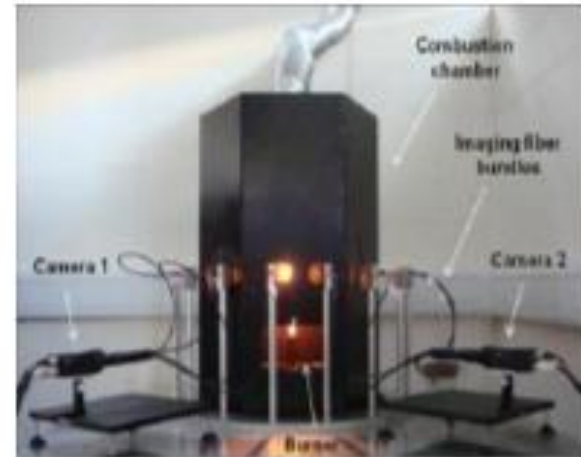
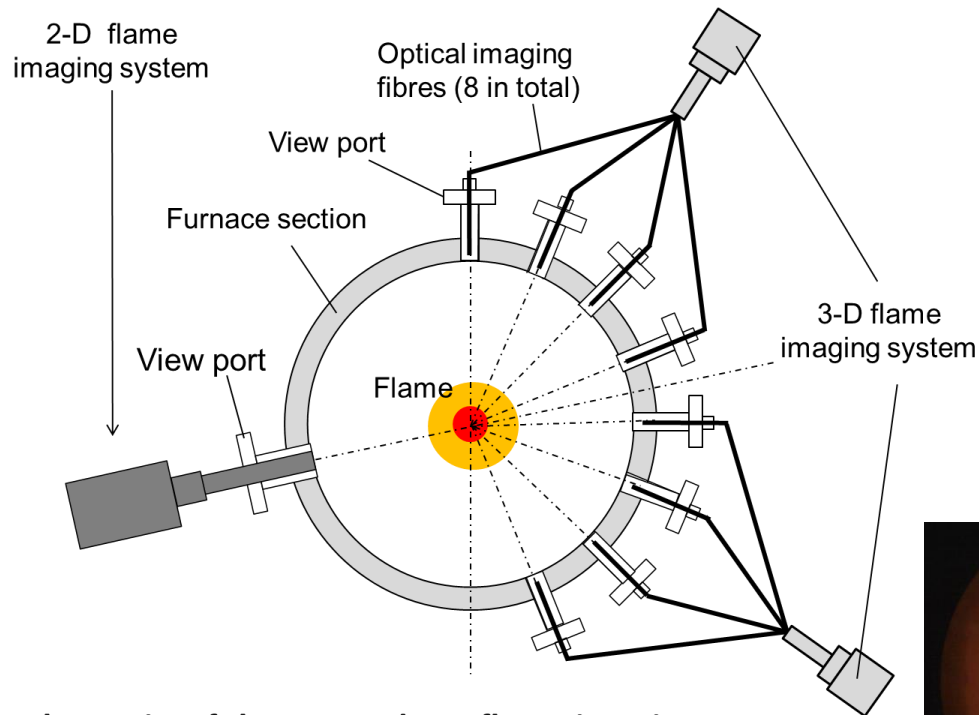
- ❑ Large Eddy Simulation of the CRIEPI Pulverised Coal Burner
- ❑ Ash transformation and deposition in oxyfuel environments



- ❑ Development of a 250 kW Solid Fuel Combustion Test Facility
- ❑ LES CFD modelling of the Oxy-fuel combustion



- ❑ 2D and 3-D Flame imaging
- ❑ Flow metering and on-line sizing of pulverised coal



Flame image and temperature distribution

Two main activities are experimental trials in a 100kW retrofitted oxy-combustor, and the development of a kinetic model using Aspen Plus

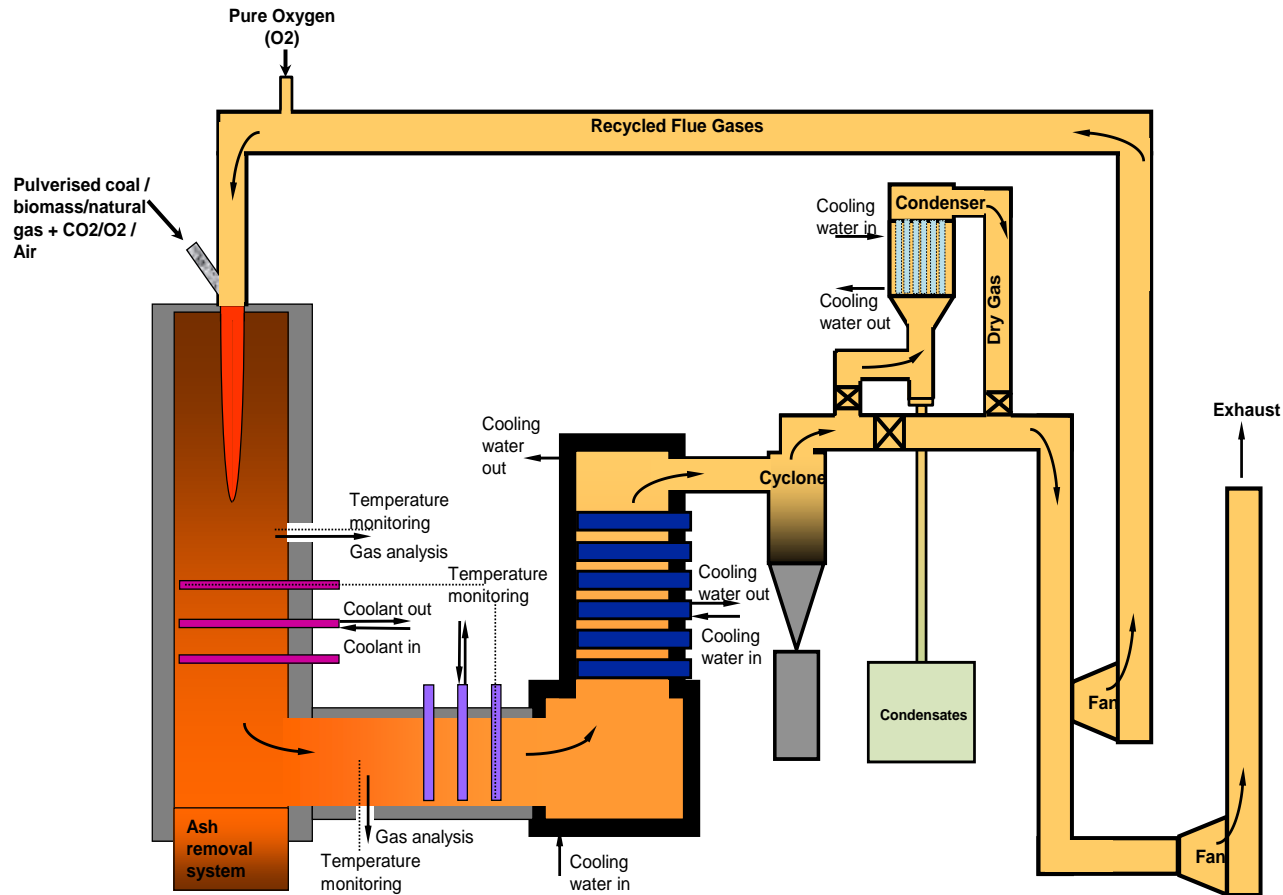
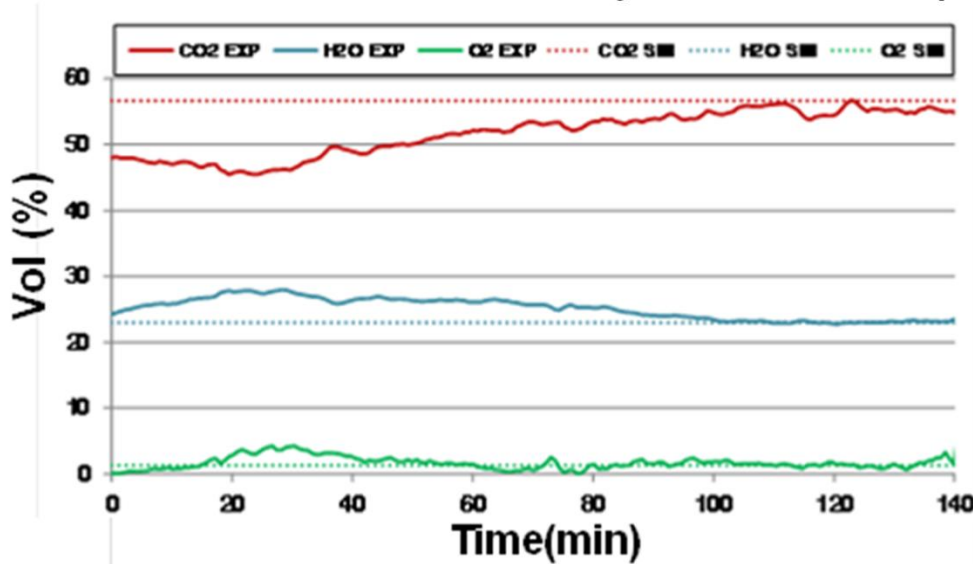


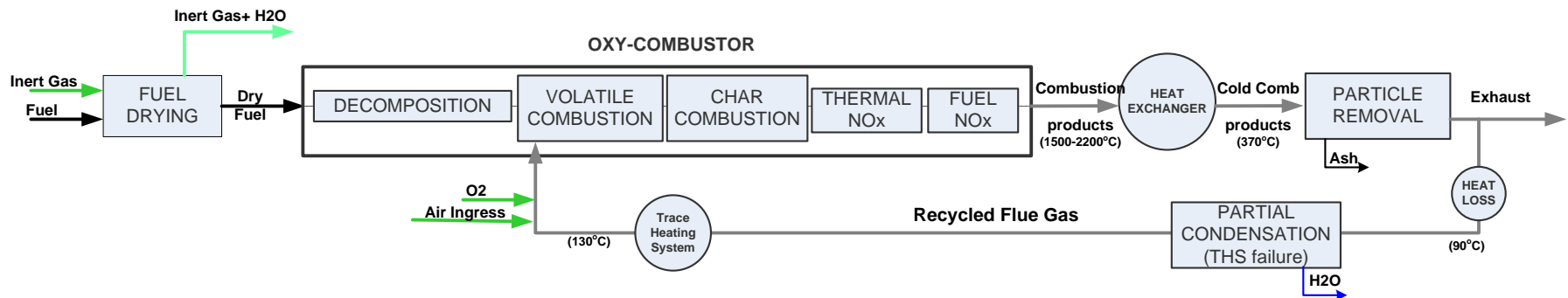
Diagram of 100kWth Oxy-Combustor with Condenser

# Experimental and Simulation data

## 100% Daw Mill Coal-52%Recycled Flue Gas (wet)



The recirculation flue gas (RFG) rate was set to be of 52% of the total flue gas. The maximum percentage of CO<sub>2</sub> observed was 56.7% wet-based (73.6% in dry-based) when 100% Daw Mill coal was fired.



Aspen Plus Box- plot of the Rate-based Model with Partial Condensation in the RFG

# Conclusions and What Next?

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## ***Oxy-Cap progress***

- new data generated on combustion behaviour, new models developed, ignition/burn-out, recycle behaviour, ash behaviour, etc.
- many new skilled researchers trained, and
- increased UK capacity for oxy-combustion research

## ***Oxy-Cap2 – ‘To accelerate progress towards achieving Operational Excellence for Flexible, Efficient, Controllable, Safe and Environmentally Sustainable Oxy-fuel fired Power Plants.’***

- Oxy-combustion burner design for new and retrofit applications
- Impacts of fuel (coal and biomass) and load changes on boiler/recycle environments and ash behaviour
- Improved understanding of the behaviour of S-, N- and metals including Hg and their impacts on corrosion, gas cleaning requirements and downstream CO<sub>2</sub> separation
- High temperature (fireside) and low temperature (acid dew-point) corrosion, improved materials and component life prediction.
- Development of predictive computational modelling integrated with a dynamic system simulation capability

# Thank you for your attention

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# PACT CO<sub>2</sub> Flow Loop Facility at Cranfield



**E.ON-EP SRC strategic partnership**

- Current configuration - >90 bar, <40 deg  
(but capable <700 bar & -50 to 150 deg) in flow mode (fluid flow rates up to 5l/min)
- High pressure observation window-provide detailed information on phase separation, hydrodynamic flows, contamination etc.
- Automated operation
- Continuous monitoring of corrosion by electro chemical noise & Linear polarization resistance
- Measurement and monitoring of physical properties- density, pH, temp, pressure
- Impurities- H<sub>2</sub>O, H<sub>2</sub>, H<sub>2</sub>S, NO<sub>x</sub>, SO<sub>2</sub> and O<sub>2</sub> etc..; dedicated MFCs to maintain the proportions



# PACT Facilities: Chemical Looping

- **Approx. 50 KW<sub>th</sub>** pilot scale chemical looping facility-**largest UK facility**
- 100 mm ID riser for chemical (adjustable height to assess the scale up effects ,7.3 m ht) and Ca looping (4.3 m ht)
- Flexible in configuration, either as
  - Twin CFB legs or
  - Single entrained flow riser with bubbling bed (2<sup>nd</sup> reactor)
- Chemical looping mode-either for **oxy-combustion or for H<sub>2</sub> production**
- Flexible controls to enable a range of operating modes
- Rig supplied with different bulk gas mixtures--**O<sub>2</sub>, CO<sub>2</sub>, N<sub>2</sub>, H<sub>2</sub> and CO**
- Dedicated **MFCs** for each bulk gas
- Dedicated safety system with controls

