



# 10<sup>th</sup> European Conference on Coal Research and its Applications

## Bond Index & Hardgrove Grindability Index Tests for Biomass & Coal

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**BF2RA**

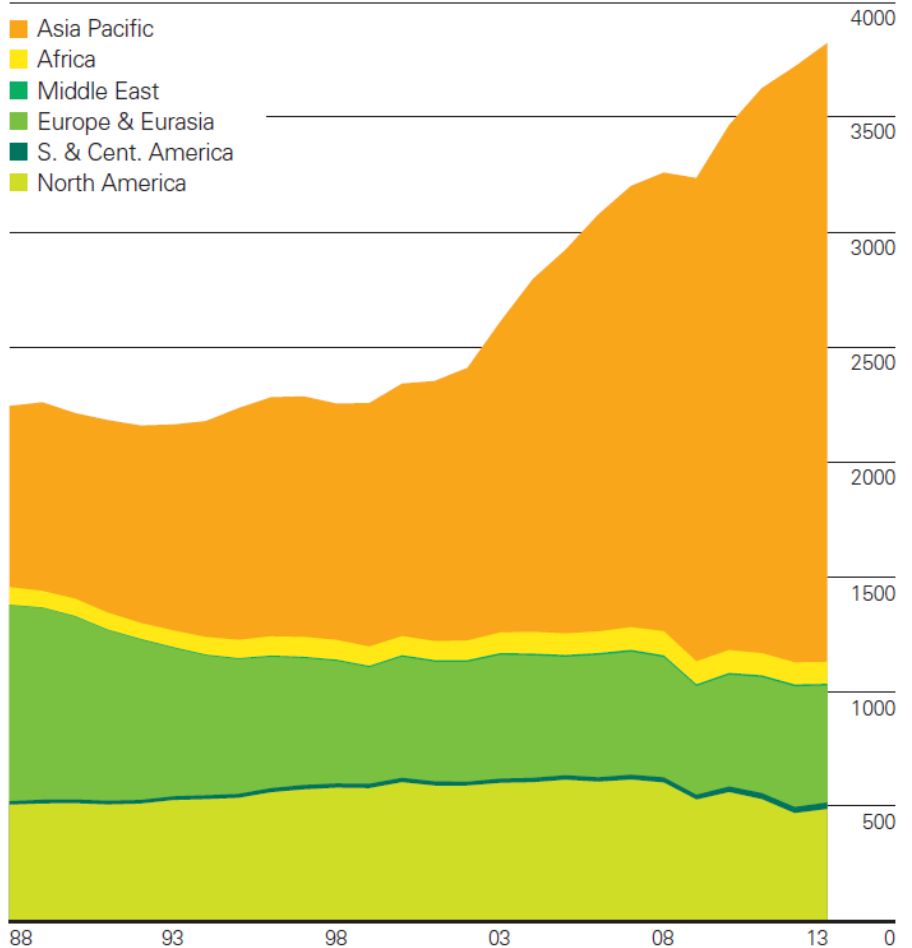


# Status of Coal

- ❑ Coal produced 36% of all UK electricity generation in 2013 [2]
- ❑ EU regulations reducing  $\text{NO}_x$ ,  $\text{SO}_x$  and particulate emissions
- ❑ UK government legally bound to cut  $\text{CO}_2$  emissions by 80% by 2050
- ❑ Nine oil and coal power plants closing by 2016 and ten nuclear power facilities to close by 2035
- ❑ Biomass co-firing reduces  $\text{NO}_x$  emissions and extends the life of coal fired plants

## Consumption by region [1]

Million tonnes oil equivalent

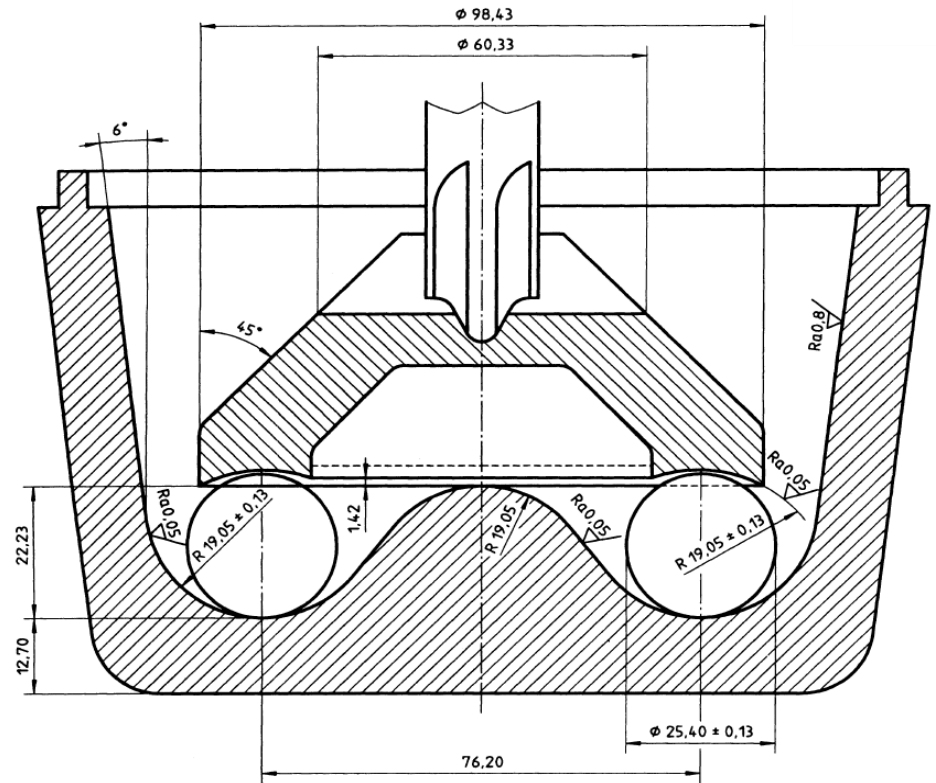


# Samples Tested



# Standard Grindability Test for Coal

- Most widely used grindability test for coal is the Hardgrove Grindability Index Test (HGI) [3]
- The HGI of binary coal blends cannot be predicted from the weighted average of the individual coals in the blend [4, 5]
- HGI values become an ineffective measure of grinding behaviour as coal properties move away from the norm [6]



# Hardgrove Grindability Index (HGI)

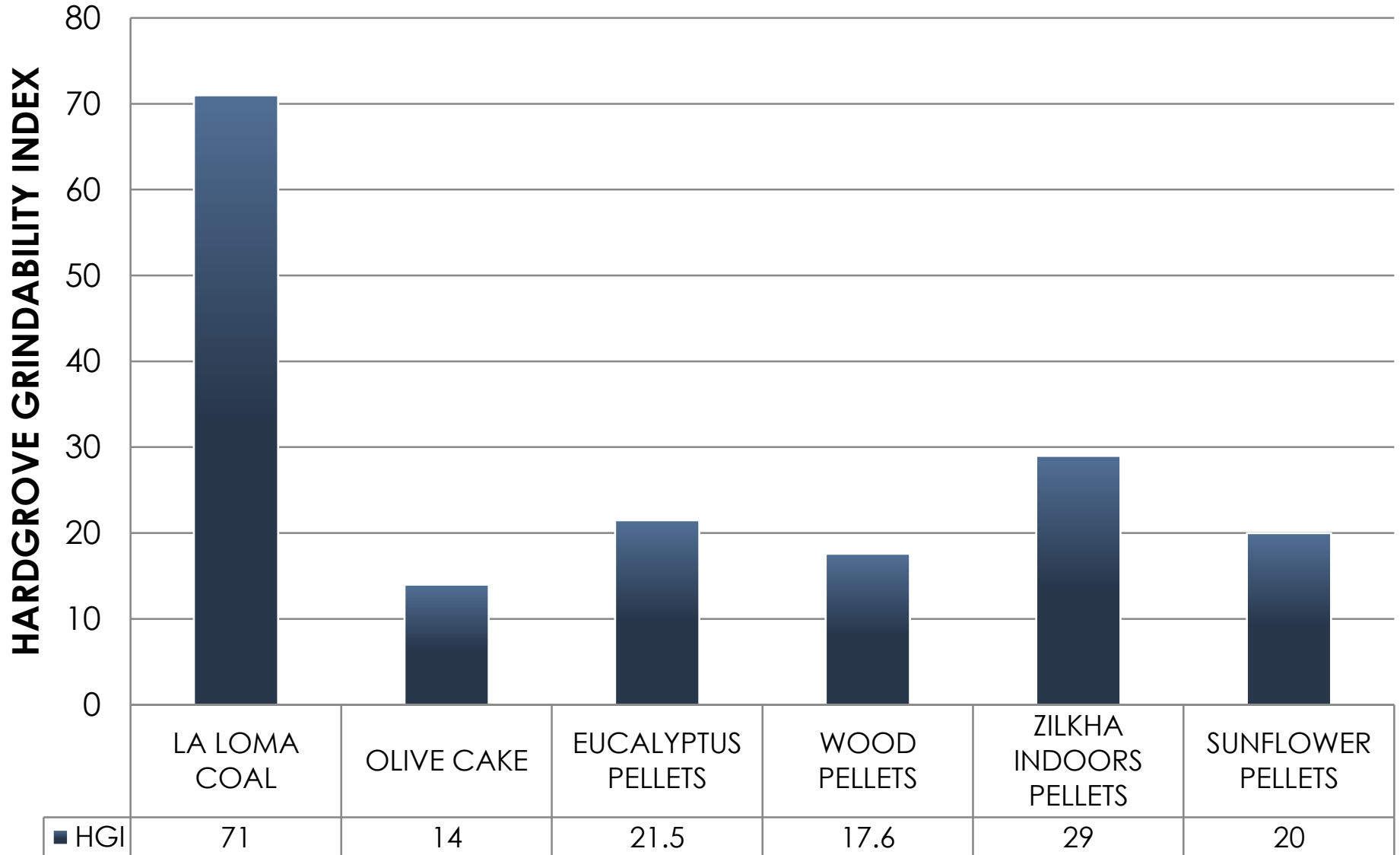
- Test conducted according to BS 1016-112:1995 [3] and conducted at Environmental Scientific Group, Bretby, UK
- 50g  $\pm$  0.01g of sample (1.18mm-600 $\mu$ m) milled for 60 revolutions.
- The sample sieved with 75 $\mu$ m sieve size and mass  $m$  (g) is calculated:

$$m = 50 - m_1$$

- where  $m_1$  is the mass (g), retained on the 75 $\mu$ m sieve.
- HGI found from calibration chart base on value of  $m$



# HGI Results



# HGI Conclusions

- ▣ HGI is a poor grindability test for biomass
- ▣ Pre milled size is unrepresentative of biomass (1.18mm-600 $\mu$ m)
- ▣ 75 $\mu$ m is too small a target particle size for biomass
- ▣ Milling is a volumetric process, and HGI favours denser materials, giving favourable results to coal like La Loma
- ▣ Good indicator of milling performance for vertical spindle mill for coal
- ▣ Potential for method to be modified in larger mill for biomass

# Theories of Comminution

All work indices are derived from the general comminution energy equation proposed by Walker et al. [7] which relates the net specific energy  $E$ , the characteristic dimension of the product  $x$ , the exponent  $n$ , and a constant  $C$  related to the material:

$$dE = -C \frac{dx}{x^n}$$

*The 3 Theories of empirical size reduction:*

- ▣ **Rittinger's:** The energy required for size reduction is proportional to the new surface area generated [8]
- ▣ **Kick's:** The equivalent relative reductions in sizes require equal energy [9]
- ▣ **Bond's:** The net energy required in comminution is proportional to the total length of the new cracks formed [10]



# Bond Index Test

- ❑ Test conducted on a Bond Index testing mill (Bico-Braun, USA)
- ❑ 700ml of sample milled for 100 revolutions.
- ❑ New number of revolutions is calculated to produce fines equal to 1/3.5 of the total charge of the mill.
- ❑ The **Bond Work Index  $W_i$** , expresses the resistance of the material to grinding to a specified product size (kWh/ton)
- ❑ The **Work Input  $W$**  gives the power required by the mill to grind the product to the required product size (kWh/ton)



# Bond Index Equations

- Bond Work Index Equation is:

$$W = 10W_i \left( \frac{1}{\sqrt{P_{80}}} - \frac{1}{\sqrt{F_{80}}} \right)$$

Where  $W$  is the work input (kWh/t),  $W_i$  is the Work Index (kWh/t), and  $F_{80}$  and  $P_{80}$  are the 80% passing size of the feed and product ( $\mu\text{m}$ ) respectively.

- Bond Work Index  $W_i$  can be found through the following equation:

$$W_i = \frac{44.5}{P_1^{0.23} G^{0.82} \left( \frac{10}{\sqrt{P_{80}}} - \frac{10}{\sqrt{F_{80}}} \right)}$$

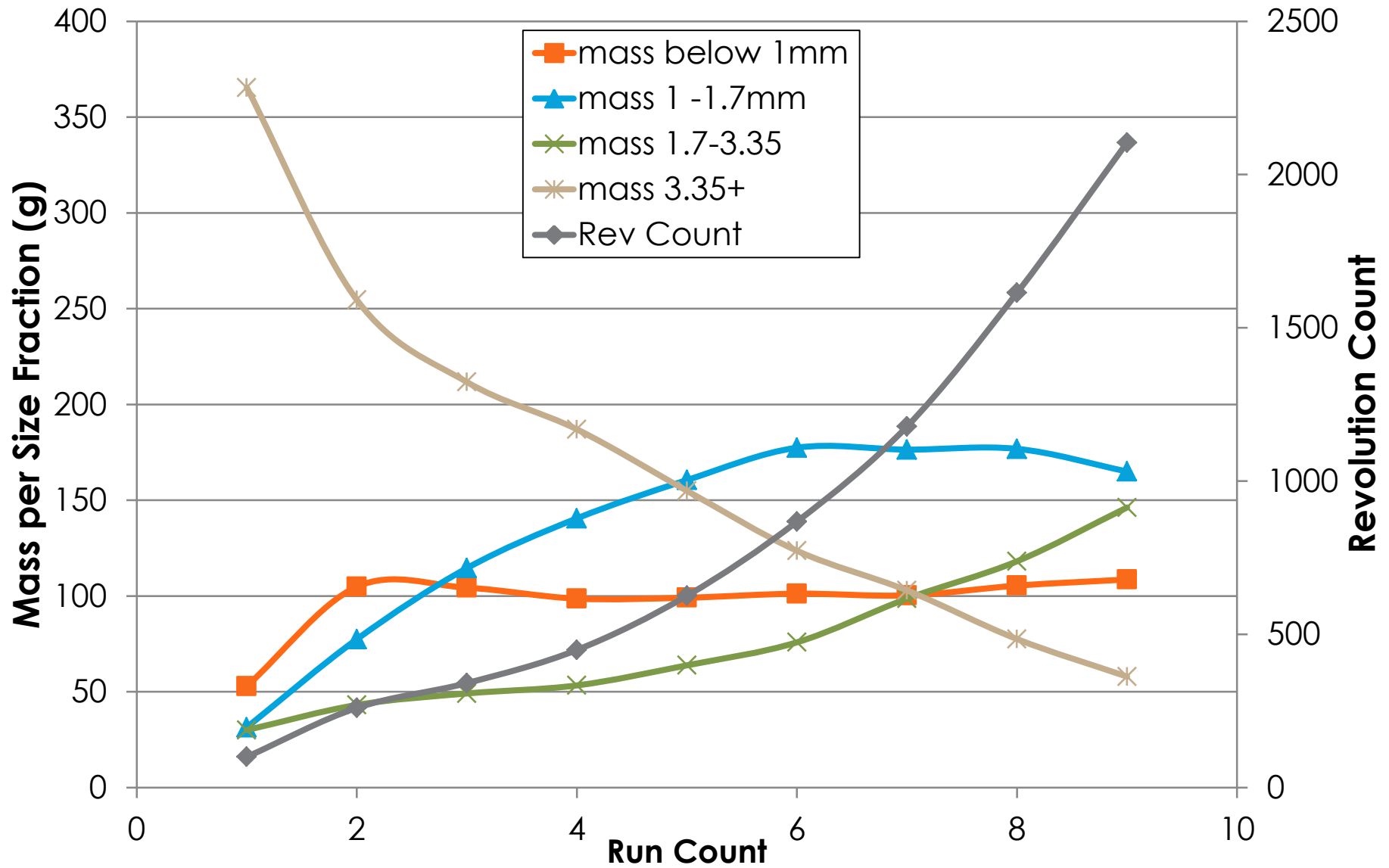
Where  $P_1$  is the target sieve size ( $\mu\text{m}$ ),  $G$  is the grindability (net g/rev).

# Bond Index Results

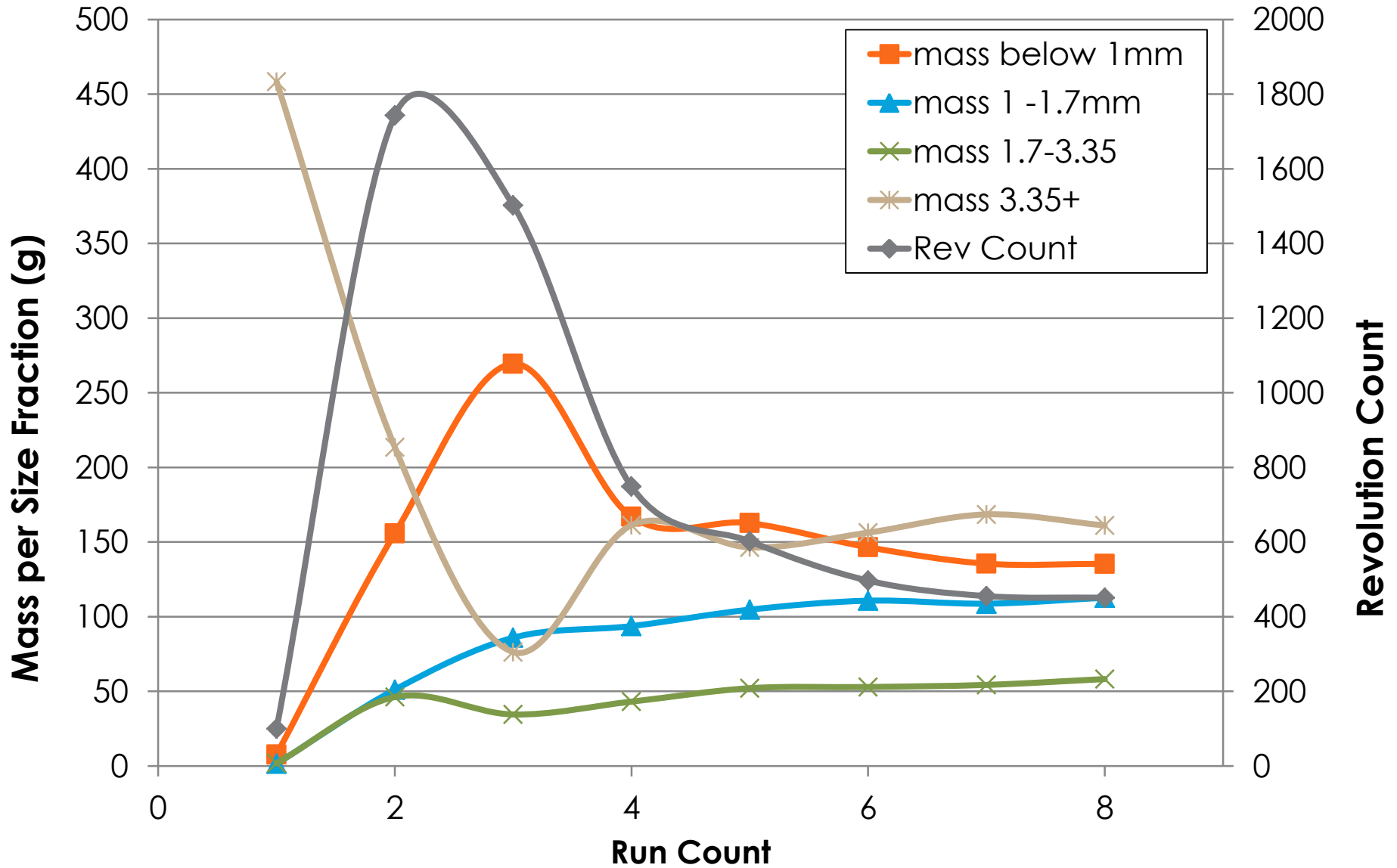
Sample	HGI	F80 (µm)	P80 (µm)	Target (µm)	Grindability per rev	Final rev count	Bond Index KWh/ton	Power to grind to product size (kWh/ton)
Wood Pellets	17.60	8400	<b>786</b>	1000	<b>0.053</b>	2141	<b>413.03</b>	102.29
Miscanthus Pellets	-	6290	<b>811</b>	1000	<b>0.057</b>	2168	<b>425.87</b>	95.85
Sunflower Pellets	20.00	8620	<b>764</b>	1000	<b>0.059</b>	1699	<b>366.32</b>	93.08
Eucalyptus Pellets	21.50	8390	<b>757</b>	1000	<b>0.340</b>	411	<b>87.28</b>	22.25
Zilkha SE Pellets	29.00	5910	<b>355</b>	1000	<b>0.283</b>	556	<b>63.86</b>	25.62
Stramproy T Pellets	-	8000	<b>758</b>	1000	<b>1.655</b>	60	<b>16.30</b>	4.10
Olive Cake	14.00	3712	<b>590</b>	1000	<b>0.202</b>	390	<b>136.24</b>	33.75
La Loma Coal	70.50	2709	<b>77</b>	90	<b>0.664</b>	242	<b>23.35</b>	22.11



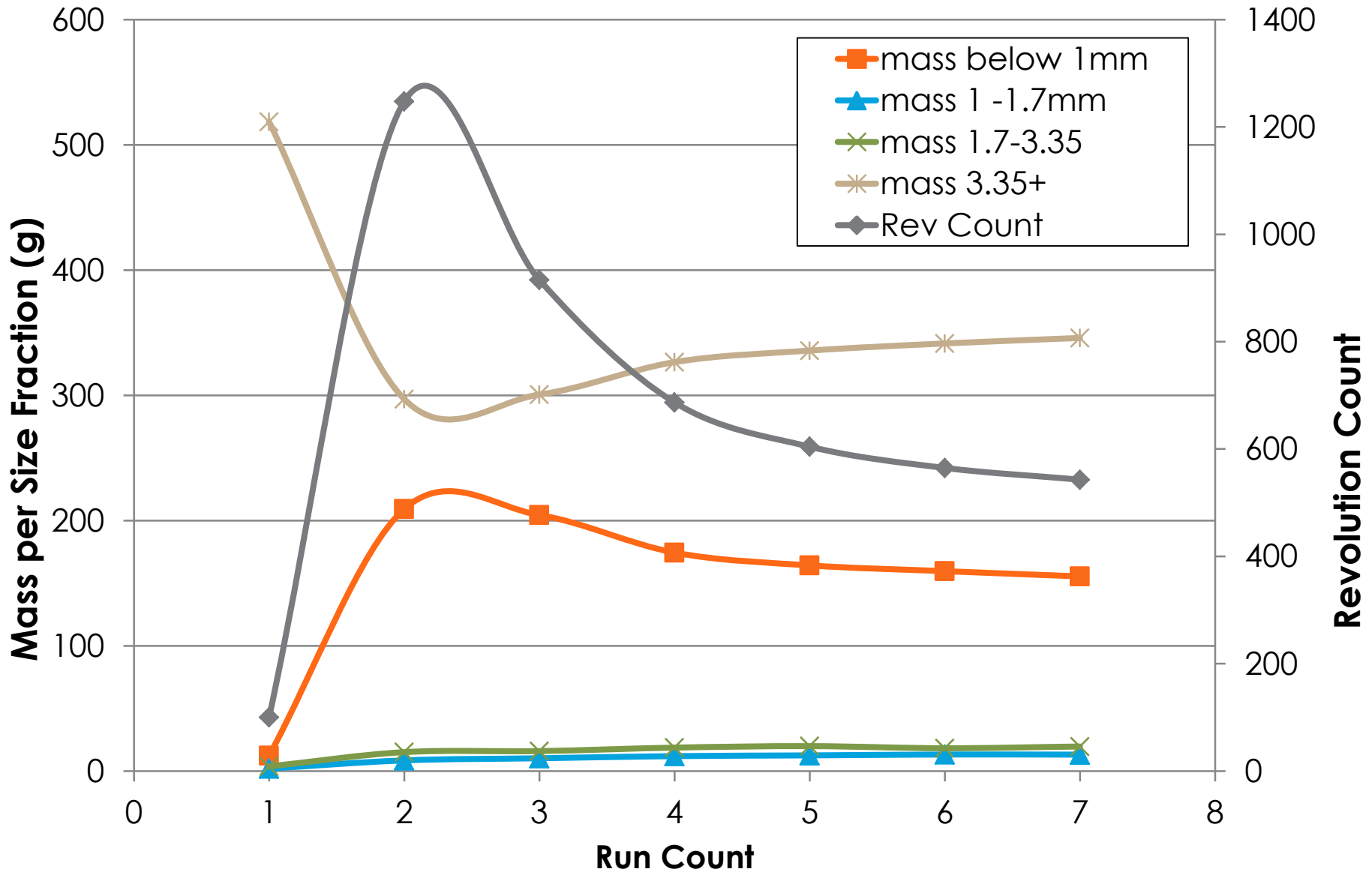
# Wood Pellets



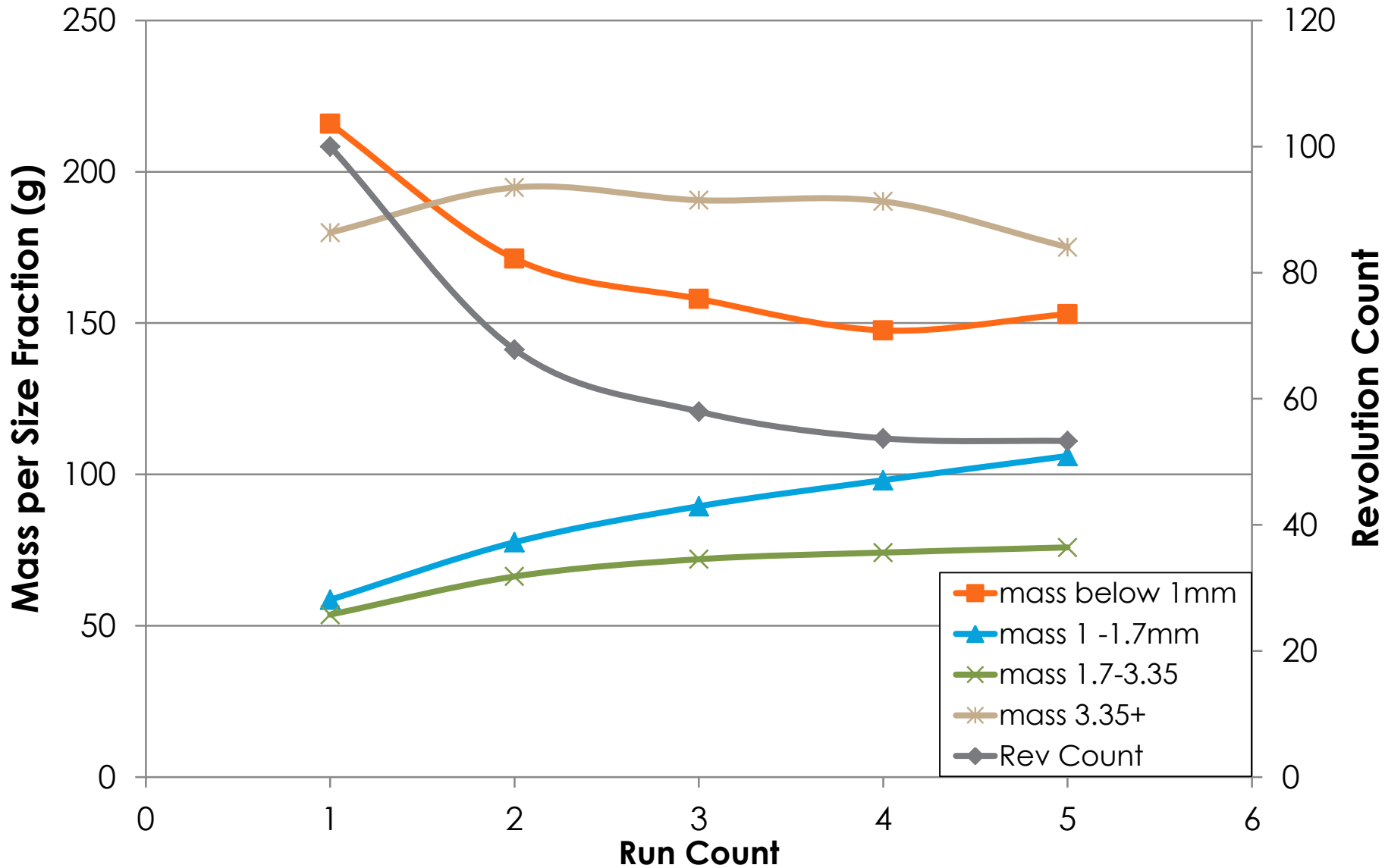
# Eucalyptus Pellets



# Zilkha Steam Exploded Pellets



# Stramproy Torrefied Pellets





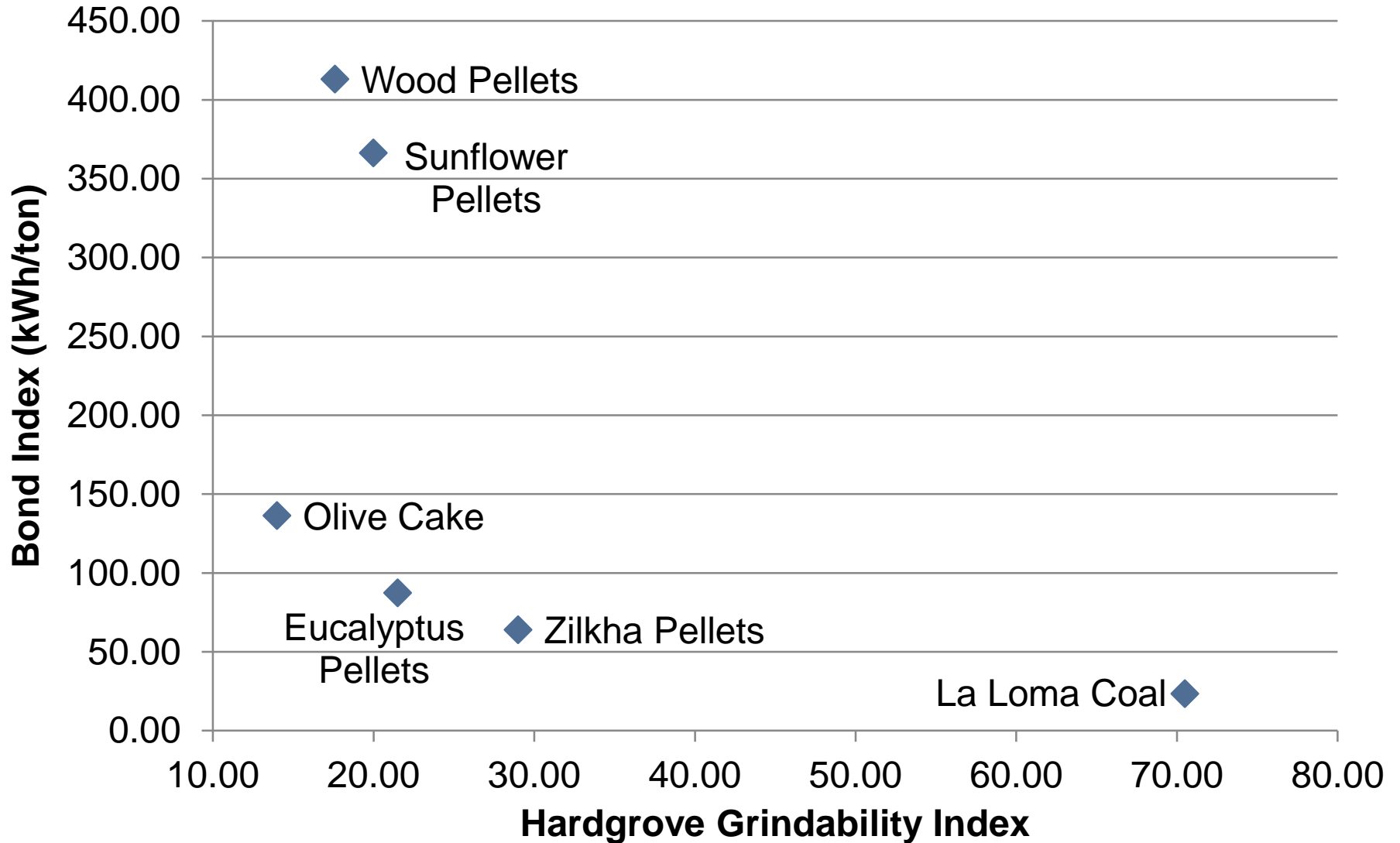
# Bond Index Conclusions

- Bond Index Test can be used on biomass to analyse the grinding performance and behaviour of biomasses in a tube and ball mill
- Allows analysis of impact of different target particle size on grindability
- Mimics mill chocking and shows impact of pellet particle size on milling behaviour
- Matching  $P_{80}$  to classifier particle size critical in optimising mill performance
- Pre-densified particle size of pellets has large impact on grindability and energy consumption in ball and tube mill

# HGI vs Bond Index Test

	<b>Bond Index</b>	<b>HGI</b>
Mill Comparison	Tube & Ball mill	Babcock mill (ring-ball)
Target Particle Size	Any size below 3.35mm	75µm
Particle Size Range	<3.35mm (powder) or pellet size	1.18mm-600µm
Mass constriction	Volume – 700ml	Mass – 50g
Output	kWh/ton	HGI Index
Suitable materials	Any	Good quality coals

# HGI vs Bond Index Test



# Conclusions & Recommendations

- ▣ HGI is a poor test of grindability for biomass
- ▣ Standard grindability test for ring-roller/ball mill is required for biomass
- ▣ Bond Index test can be used for biomass for analysing grinding performance of biomass in tube and ball mill
- ▣ Matching  $P_{80}$  to classifier particle size critical in optimising mill performance
- ▣ Pre-densified particle size of pellets has large impact on grindability and energy consumption in ball and tube mill
- ▣ Need to improve pellet specifications to ensure pre-densified particle size is close to the classifier target size

# Thank you for listening

The author would like to thank the University of Nottingham, the Biomass and Fossil Fuel Research Alliance (BF2RA), and EDF Energy plc for their support during this project.

**Questions?**

# References

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[10] Bond FC. The Third Theory of Comminution. *Trans AIME* 1952;193:484–94.